

Conclusion

In view of the present Response and the Response filed on September 20, 2002, reconsideration of the claims and allowance of the subject application is earnestly solicited. The Examiner is invited to contact the undersigned at the below-listed telephone number, if it is believed that prosecution of this application may be assisted thereby.

Respectfully submitted,

BURNS, DOANE, SWECKER & MATHIS, L.L.P.

By: Mel. M. Hayworth
Melissa M. Hayworth
Registration No. 45,774

P.O. Box 1404
Alexandria, Virginia 22313-1404
(919) 941-9240

Date: Dec. 4, 2002

Amendment dated December 4, 2002

Marked up Specification

Page 6, Line 33

The lighter fraction typically comprises a mixture of hydrocarbons, including mono-olefins and alcohols. The mono-olefins are present in an amount of at least about 5.0 wt % of the lighter fraction, preferably at least about 15.0 wt % of the lighter fraction, and most preferably at least about 25.0 wt % of the lighter fraction. The mono-olefins boil at a temperature in the range of about -105°C to about 350°C. The alcohols are present in an amount typically of at least about 0.5 wt % or more. The alcohols boil in a temperature range of about 50°C to about 350°C. The lighter fraction typically boils at a temperature of from about -65°C to about 350°C.

Amendment dated December 4, 2002

Marked up Specification

Page 9, Line 2 and prior to the paragraph beginning on Page 9, Line 14:

In one embodiment, a first hydrogen-containing gas is added to a hydrocarbon stream in an amount sufficient to reduce the amount of heavy molecular weight products formed during heating as compared to a heated hydrocarbon stream without added hydrogen, to form a mixed stream. The mixed stream is heated, preferably to a temperature in the range of from about 120°C to about 400°C, and a second hydrogen-containing gas is added to the heated mixed stream in an amount, preferably more than 750 SCFB, sufficient to effect hydroconversion of the mixed stream to form a hydroconversion feed stream. The hydroconversion feed stream is heated to the reaction temperature, preferably to a temperature in the range of 250°C to about 400°C, and the hydroconversion feed stream is hydroconverted.